DEVELOPMENT OF CHEMICAL PROCESSES

Herbert Vogel

Ernst-Berl-Institut für Technische und Makromolekulare Chemie, Technische Universität Darmstadt, Germany.

Keywords: Chemical Engineering, Chemical Industry, Raw Materials, Intermediates, Life Cycles, Chemical Thermodynamics, Chemical Kinetics, Hydrodynamics, Catalysis, Chemical Reactors, Thermal Separation Processes, Process Development, Miniplant, Microplant, Pilot plant, Process evaluation, Investment costs, Production costs.

Contents

- 1. Introduction
- 2. Scientific Basics of Process Development
 - 2.1. Physical-chemical Data
 - 2.2. Thermodynamics
 - 2.3. Chemical Kinetics
 - 2.4. Hydrodynamics
- 3. The Components of a Chemical production Plant
 - 3.1. Catalyst
 - 3.2. Chemical Reactor
 - 3.3. Separation Processes
- 4. Standard Approach of Process Development
 - 4.1. Process Development as an Iterative Process
 - 4.2. Putting up an Initial Version of the Chemical Process
 - 4.3. Testing of the Single Process Steps
 - 4.4. Microplants
 - 4.5. Checking the Integrated Process in a Miniplant
 - 4.5.1. Miniplant Technology
 - 4.5.2. The Pilot Plant
- 5. Execution of a Project
- 6. Evaluation of Chemical Processes
 - 6.1. Preparation of Study Reports
 - 6.2. The Evaluation of the Investment
 - 6.3. The Evaluation of the Production Costs
- 7. The Future of the Process Development

Glossary

Bibliography

Biographical Sketch

Summary

The task of the process development and of the chemical engineering respectively is, to extrapolate a chemical reaction discovered and researched in the laboratory to an industrial scale, taking into consideration the economic, safety, and ecological boundary conditions.

The starting point is the laboratory equipment and the outcome of development is the production plant; in between, process development is required. The development of chemical processes is a complex procedure; therefore it does not take place in a one-way street. Assumptions are made for the individual development stages which are only confirmed or refuted when the next stage is being worked on. It may be necessary, therefore, to go through the individual stages several times with modified assumptions, resulting in a cyclic pattern. The first hurdle in establishing a new process is overcome when a promising synthetic route, usually with associated catalysts, is discovered. The conventional process development is carried out in three stages:

- Optimized laboratory synthesis
- Laboratory plant (the so called miniplant
- Pilot plant.

The scale-up factor from one stage to the next is always limited by the "minimum principle", i.e., the process stage or piece of equipment with the lowest scale-up feasibility determines the maximum capacity of the next larger plant whose operating performance can be calculated. It is here that the engineer has an opportunity to save time and money. Consequently, efforts are now made to extrapolate directly from the miniplant to the production scale. An important tool to do this is the so-called integrated-miniplant-technology. This means the synergism between:

- Process pre-selection via microplants and process evaluation via short cut methods.
- Experiments via a continuously operating miniplant which includes all the recycling paths.
- Mathematical simulation of the experiments.

So, safety in scaling up is as good as that obtained by setting up a pilot plant.

1. Introduction

Chemical engineering is the science that deals with the development of chemical processes from a small-scale laboratory reaction vessel to a large-scale production process under economic, safety, ecological, and juristic boundary conditions. The chemical engineer has to develop and to improve the quality of the corresponding technical tools.

The bases of chemical engineering are:

- Mathematics
- Natural science such as physics, chemistry and biology
- Engineering science, especially mechanical and electrical engineering
- Business administration, especially cost accounting.

The basis was founded by important people such as:

• Sadi Carnot, French physicist (Thermodynamics of combustions in steam engines)

- *Rudolf Clausius*, German physicist (Thermodynamics of chemical systems at molecular scale)
- *Josiah Willard Gibbs*, American scientist (Developed much of the theoretical foundation that led to the development of chemical thermodynamics)
- *Hermann von Helmholtz*, German scientist (Thermodynamics of electrochemical processes)

Henry E. Armstrong offered the first course in Chemical Engineering at the Imperial College in London in *1885. George E. Davis* produced the first Handbook of Chemical Engineering in *1901.*

The difference between laboratory and industrial chemistry can be highlighted by the following simple example:

The polymerization of acrylic acid takes place in a round bottom flask (5 cm diameter) and a production vessel (spherical, 2 m diameter). The heat of polymerization is 77.4 kJ mol⁻¹. The geometric parameters and heat produced for the reaction are shown in Figure 1.

The example shows that the heat liberated for the reaction on the laboratory scale can easily be removed by water cooling, whereas in the case of the production scale, the heat liberated will cause the vessel to explode.

	Lab apparatus	Production plant
	\bigcirc	
Diameter d	5 cm	2 m
Volume V	65.5 cm ³	4.19 m ³
Surface A	8.5 cm ²	12.6 m ²
Specific surface area a	120 m ² m ⁻³	3 m ² m ⁻³
Mass of acrylic acid m	68.0 g	4.36 t
Liberated heat Q	0.020 kWh	1 300 kWh
Specific heat charges $Q_{\rm spec}$	2.55 kWh m ⁻²	103.5 kWh m ⁻²

Figure 1. Geometric and heat production conditions for the both cases: Lab scale and production scale. The heat flux density for water cooling is typically in the order of magnitude of 10 kW m^{-2} .

If we look at the production structure of the chemical industry from a bird eye view, it is seen that there are only a few hundred major basic products and intermediates which are

produced on a scale of at least a few thousand to several million tones per annum worldwide. This so called building-blocks or intermediates, which are in turn produced from only about ten raw materials (especially crude oil), are the stable foundation on which the many braches of refining chemistry (dyes, pharmaceuticals, etc.), with their many thousands of often only short-lived consumer products, are based. This has resulted in the well-known "*ChemisTree*" (Figure 2).

A special characteristic of the basic products and intermediates is their longevity. They are statistically so well protected by their large numbers of secondary products and their wide range of possible uses that they are hardly affected by the continuous changes in the range of products on scale. Unlike many end products, which are replaced by better ones in the course of time, they do not themselves have a life cycle. However, the processes for producing them are subject to change. This is initiated by new technical possibilities and advances opened up by research, but are also dictated by the current raw material situation.



Figure 2. Example for a so called *ChemisTree*: starting from the raw material crude oil and progressing through the basic products and intermediates, to the refined chemicals and final consumer products, as well as specialty chemicals and materials.

In the longer term, an oil shortage can be expected in 40 to 50 years, and this will result in increased use of natural gas or biomass. The fossil raw material with the longest future is coal, with reserves for more than 200 years. The question whether natural gas reserves in the form of methane hydrate, in which more carbon is stored than in other fossil raw materials, will be recoverable in the future cannot be answered at present, since these lie in geographically unfavorable areas.

In the case of basic products and intermediates it is not the individual chemical product but the production process or technology which has a life cycle (Figure 3): To remain competitive at this point the producer must be the price leader for his process. Therefore, strategic factors for success are:

- Efficient process technology
- Exploiting economy of scale by means of world-scale plants
- Employing a flexible integrated system at the production site
- Professional logistics for large product streams.



Figure 3. Life cycles of the Ethylene oxide process. In 1999 the ethylene oxide production in the U.S. was over 4 Mio. t a⁻¹ [Weissermel 2003].

The demands made on process development for fine chemicals differ considerably from those of basic products and intermediates. In addition to the boundary conditions of better and/or cheaper, time to market (production of the product at the right time for a limited period) and focused R&D effort are of importance here. Further strategic factors for success are:

- Development partnerships with important customers
- The potential to develop complex multi step organic syntheses
- A broad technology portfolio for the decisive synthetic methods
- Certified pilot and production plants
- Reputation as a competent and reliable supplier.

Special chemicals are complex mixtures whose value lies in the synergistic action of their ingredients. Here the application technology is decisive for market success. The manufacturer can no longer produce all ingredients, which can lead to a certain state of dependence. Strategic factors for successful manufacturers are:

- Good market knowledge of customer's requirements.
- A portfolio containing numerous magic ingredients
- Good technical understanding of the customers systems
- Technological breadth and flexibility.

Active substances such as pharmaceuticals and agrochemicals can only be economically marketed while they are under patent protection, before suppliers of generic products enter the market. Therefore, producers of such products cannot simply concentrate on costly research. As soon as possible after clinical trials and marketing approval, worldwide scales of the product must begin so that the remaining patent time can be used for gaining customers. In contrast, the actual chemical production of the active substance is of only background importance. The precursors can be farmed out to other companies. Strategic factors for success of active substance manufacturers are:

- Research into bimolecular causes of disease and search for targets for pharmacological activities
- Efficient development of active substances (high-throughput screening, searching for and optimizing basic structures, clinical development)
- Patent protection
- High-performance market organization.

Enterprises which already have competitive advantages must take account of the technology –S-curve in their research and development strategy (Figure 4).



Figure 4. Technology-S-curve: Productivity of R&D expenditure increases considerably on switching from basic technology (_____) to a new trend setting technology (-----).

The curve shows that as the research and development expenditure on a given technology increases, the productivity of this expenditure decreases with time. If enterprises are approaching the limits of a given technology, they must accept disproportionately high research and development expenditure, with the result that the contribution made by these efforts to the research objectives of cheaper and /or better becomes increasingly small, thereby always giving the competitor the opportunity of catching up on the technical advantage. On the other hand, it is difficult for a newcomer to penetrate an established market. But, as Korean or Chinese companies have shown in the past, it is not impossible.

Once an enterprise has reached the upper region of the product or technology-S-curve, the question arises whether it is necessary to switch from the standard technology to a new pace-setting technology in order to gain a new and sufficient competitive advantage. Figure 3 depicts this switch to a new technology schematically and shows that on switching from a basic technology to a new pace-setting technology, the productivity of the research and development sector increases appreciably, and substantial competitive advantages can thus be achieved.

The potential of old technologies for the development of cheaper and/or better are only small, whereas new technology have major potential for achieving competitive advantages. It is precisely on this innovative activity that the prosperity of highly developed countries with limited raw material sources such as the European union and

Japan is based, since research represents an investment in the future with calculable risks, whereas capital investments in the present are based on existing technology.

To assess whether a research and development strategy of better and/or cheaper is still acceptable in the long term for a given product or production process, the R&D management must develop an early warning system that determines the optimum time for switching to a new product or a new technology. Here it is decisive to have as much up-to-date information on competitors as possible. This information can be obtained not only from the patent literature but also from external lectures, conferences, company publications, and publicly accessible documents submitted to the authorities by competitors. Since industrial research is very expensive, instruments for controlling the research budget are required, for example:

- A cost/benefit analysis for the particular product area, whereby the benefit is determined by the corresponding user company sector.
- A portfolio analysis to answer the questions:
 - Where are we now?
 - Where do we want to be in 12 years?
 - What do we have to do to now to get there?
- An ABC analysis for controlling the R&D resources, based on the rule of thumb that
 - o 20 % of all products account for 80 % of turnover, or
 - o 20 % of all new developments account for 80 % of development costs.

It is therefore important to recognize which 20 % these are in order to set the appropriate priorities (A = important, profitable, high chance of success; B = low profitability; C = less important tasks with low profitability).

The ways in which chemical companies organize their research varies and depend on the product portfolio. Mostly it involves a mixture of the two extremes: pure centralized research on the one hand, and decentralized research on the other.

The task of process development is to extrapolate a chemical reaction discovered and researched in the laboratory to an industrial scale, taking into consideration the economic, safety, ecological, and juristic boundary conditions. The starting point is the laboratory apparatus, and the outcome of development is the production plant; in between, process development is required [Dittmeyer 2003, Storhas 2003, Ullmann 2002, Vogel 2002, 2005].

TO ACCESS ALL THE **55 PAGES** OF THIS CHAPTER, Visit: <u>http://www.eolss.net/Eolss-sampleAllChapter.aspx</u>

Bibliography

Armor J.N. (1996). Global Overview of Catalysis, *Applied Catalysis A: General* **139**, 217-228. [This presents a number of key challenges for catalysis in the future such as ultra high selectivity, the construction of active sites at the molecular level, in-situ analytical methods etc.]

Baerns M. (2006). *Technische Chemie*, Weinheim: Wiley-VCH. [The classical textbook for all fields of technical chemistry such as chemical reaction engineering, basic unit operations and production processes in chemical industry].

Bartholomew C. H. (1994) Catalytic reactor design, *Chemical Engineering* 70-75. [This presents the design principles for a heterogeneous catalyst and the reactor such as material balances, energy balances and kinetic rate expression].

Behr A. (2000) Miniplants, *Chem.-Ing.-Tech.* **72**, 1157-1166. [This work describes the important tasks of a miniplant, namely, the investigation of the recycling streams and the scale-up problem].

Berty B. J. M. (1979) The Changing Role of the Pilot Plant, *CEP* **9**, 48-50. [Once a place to collect or generate data for correlations, the pilot plant unit is now a place to test experimental results from bench work or models and to check design calculations].

Bisio A. (1997) Catalytic process development, *Catalysis Today* **36**, 367-374. [The catalysis process development is described from a process designer's point of view].

Blaß E. (1985) Methodische Entwicklung verfahrenstechnischer Prozesse, *Chem.-Ing.-Tech.* **57**, 201-210. [This describes a brief introduction to the system concept and the application of the system engineering procedural model to process development].

Blaß E. (1989) *Entwicklung verfahrenstechnischer Prozesse Frankfurt*: Otto Salle Verlag. [This describes the development of technical processes, methods, guidance, solution searching and solution selection].

Buschulte K. (1995) Verfahrensentwicklung durch Kombination von Prozeßsimulation und Miniplant-Technik *Chem.-Ing.-Tech.* **67**, 718-723. [This article demonstrates the importance of process simulation in the individual phases of process development].

Buzzi-Ferraris G. (1999) Planning of experiments and kinetic analysis, *Catalysis Today* 52, 125-132. [In this paper the authors have taken into account the distinct phases necessary to build a kinetic model. In particular, several mistakes that can be made during such activity are described and analyzed].

Christmann A. (1985) Integrierte Verfahrensentwicklung, *Chem. Ind.* 37, 533-537. [This paper represents how safety and environmental protection aspects can be integrated in the process development].

Claus P. (2006) Die Rolle der Chemokatalyse bei der Etablierung der Technologieplatform Nachwachsende Rohstoffe, *Chem.-Ing.-Techn.* **78**, 991-1012. [This work deals with the development of new chemical processes based on biomass as a sustainable raw material with the help of chemocatalysis].

DAdda M. (1997) Fixed-capital cost estimating, *Catalysis Today* 34, 457-467. [The scope of cost estimating activities is to calculate the cost of facilities, which is the sum of all direct and indirect costs incurred in planning and building a plant ready for the start-up].

Damköhler G. (1936) Einflüsse der Strömung, Diffusion und des Wärmeüberganges auf die Leitung von Reaktionsöfen, *Ztschr. Elektrochemie* **42**, 846-862. [This classical work deals with the question, how a chemical process can be carried over from a lab scale to a production scale].

Deibele L. (2006) *Miniplant-Technik*, Weinheim: Wiley-VCH. [This book describes the requirements of running a miniplant successfully].

Dittmeyer R. (2003) *Winnacker-Küchler: Chemische Technik*, Weinheim: Wiley-VCH, 5. Auflage, 9 Bände. [This is the thesaurus in all fields of technical chemistry].

Ehrfeld W. (2000) *Microreactors*, Weinheim: Wiley-VCH. [This book describes the new micro reactor technology for all aspects of modern chemistry].

Ertl G. (2008) *Handbook of Heterogeneous Catalysis*, Weinheim: Wiley-VCH. [This is the thesaurus in all fields of heterogeneous catalysis].

Forni L. (1997) Laboratory reactors, *Catalysis Today* 34, 353-367. [The goal of this contribution is to describe the most significant apparatuses usually employed in intensive laboratory experimentation].

Glasscock D. A. (1994) Process Simulation: the art and science of modeling *Chem. Engng.* **11**, 82-89. [This paper describes how process simulation can replace pilot scale experiments].

Heimann F. (1998) Labor- und Miniplanttechnik, *Chem.-Ing.-Tech.* 70, 1192-1195. [This article deals with the equipment, which is necessary to build a miniplant].

Helmus F. P. (2003) *Anlagenplanung*, Weinheim: Wiley-VCH. [All activities which are necessary for the planning, erection, commissioning and start-up of a chemical plant are described].

Hessel V. (2002) Mikroverfahrenstechnik, *Chem.-Ing.-Tech.* **74**, 17-30 and 381-400. [This paper touches on recent developments on new components for microplants].

Hessel V. (2003) Microchemical Engineering: Components, Plant Concepts, User Acceptance – Part II, *Chem. Eng. Technol.* **26**, 391-408. [This paper touches on recent developments on new components for microplants. An important point is the analysis of possible plant concepts for microreactors].

Jakubith M. (1998) *Grundoperationen und chemische Reaktionstechnik*, Weinheim: Wiley-VCH. [This book gives a good overview about the main disciplines for a chemical engineer].

Johnstone R. E. (1957) *Methods in Chemical Engineering Pilot Plants, Models and Scale-up*, New York: McGraw Hill. [This book gives a good overview about the methods how pilot plants can be scaled-up].

Jung J. (1983) Aspekte der Vorausberechnung von Anlagenkosten bei der Projektierung verfahrenstechnischer Anlagen, *Chemie-Technik* **12**, 9-18. [This article represents a choice of investment costs methods for every planning phase.].

Kampe P. (2007) Heterogeneously catalyzed partial oxidation of Acrolein to acrylic acid, *PCCP* **9**, 3577-3589. [The major objective of this research project was to reach a microscopic understanding of the structure, function and dynamics of V–Mo–(W) mixed oxides for the partial oxidation of acrolein to acrylic acid].

Lowenstein J. G. (1985) The Pilot Plant, *Chemical Engineering* **9**, 62-76. [This article should be useful if you are involved in a pilot-plant project].

Muthmann E. (1984) Ermittlung der Investitionskosten von Chemieanlagen in verschiedenen Projektphasen *Chem.-Ing.-Tech.* **56**, 940-941. [This represents the procedure of cost estimation in the chemical large scale industry].

Robbins L. A. (1979) *The Miniplant Concept*, **CEP** 45-47. [This is a basic guide for miniplant design and operation].

Sattler K. (1995) *Thermische Trennverfahren*, Weinheim: VCH. [A classical textbook about all thermal separation processes such as rectification, extraction, absorption, crystallization etc.].

Sattler K. (2000) Verfahrenstechnische Anlagen Planung, Bau und Betrieb, Weinheim: Wiley-VCH, Band 1 und 2. [This book describes the state-of-the-art in the fields of planning, processing, erection, commissioning and start-up of chemical production plants].

Schuler H. (1995) *Prozeßsimulation*, Weinheim: VHC. [This describes how chemical processes can be simulated].

Seider W. (1999) Process Design Principles, New York: John Wiley & Sons, Inc. [A principal objective of this courseware is to describe modern strategies for the design of chemical processes].

Sowa Ch. J. (1997) Process Development: A Better Way, *Chemical Engineering Progress* 109-112. [Three key elements of a successful process development are discussed, namely, teamwork, the use of simulation tools and the use of custom manufacturing].

Storhas W. (2003) *Bioverfahrensentwicklung*, Weinheim: Wiley-VCH. [An overview about the systematical development of biochemical processes].

Ullmann (2002) *Encyclopedia of Industrial Chemistry*, Weinheim: Wiley-VCH, 6th edition. [This is the classical encyclopedia of industrial chemistry].

Vogel G. H. (2002) *Verfahrensentwicklung*, Weinheim: Wiley-VCH. [This book describes the scientific and engineering basic principles which are necessary for planning and building a chemical production plant based on a chemical laboratory concept. Furthermore, the different steps in process development and cost estimation are described].

Vogel G. H. (2005) *Process Development*, Weinheim: Wiley-VCH. [This book describes the scientific and engineering basic principles which are necessary for planning and building a chemical production plant based on a chemical laboratory concept. Furthermore, the different steps in process development and cost estimation are described].

Vogel H. (2007) Rohstoffwandel. *Chem.-Ing.-Techn.* **79**, 516-520. [An overview of the chemical raw materials of the future].

Wedler G. (2004) *Lehrbuch der Physikalischen Chemie*, Weinheim: Wiley-VCH. [The classical textbook of physical chemisty].

Weissermel K. (2003) *Industrial Organic Chemistry*, Weinheim: Wiley-VCH, 4. ed. [This book gives a quick overview of the manufacturing processes of the most important products of the chemical industry].

Wijngaarden J. (1998) *Industrial Catalysis*, Weinheim: Wiley-VCH. [This book is addressed to the developer and user of catalysts who deal with design, function and optimization of the chemical reactors in which heterogeneous catalysis is carried out. The chemical aspects of the catalysis are explained for engineers as well as the technical aspects for chemists].

Wilson G. T. (1971) Capital investment for chemical plant, *Brit. Chem. Eng. Proc. Tech.* **16**, 931. [An empirical model is presented, which is able to estimate the capital investment in an early stage of a project evaluation].

Wörz O. (1995) Process development via a miniplant, *Chemical Engineering and Processing* **34**, 261-268. [The main reason for operating a miniplant is to study recycle loops. This article shows how the accumulation of a contaminant by recycling depends on the cumulative residence time].

Zlokarnik M. (2003) Scale-up und Miniplants, *Chem.-Ing.-Tech.* **75**, 370-375. [This discusses how the experimental results from a miniplant are able to be assigned to a technical scale].

Biographical Sketch

Herbert Vogel was born in 1951 near Frankfurt/Main, Germany, and served an apprenticeship at Röhm&Haas before going on to study chemical engineering at Darmstadt Polytechnic and chemistry at Technische Hochschule Darmstadt, Germany, where he received his PhD under Alarich Weiss in physical chemistry. Between 1982 and 1993 he was employed at BASF Aktiengesellschaft in Ludwigshafen, Germany, working on the development, planning, construction and installation of petrochemical production plants. In 1993, he succeeded Fritz Fetting as professor for Technical Chemistry at the Technische Universität Darmstadt. His research interests are heterogeneous catalysis, chemistry in supercritical fluids and renewable primary products.